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CONCURRENT ISOMERIZATION AND DISPROPORTIONATION OF OLEFINS. ;

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ABSTRACT:

A catalyst composition for use in a process for the concurrent isomerization and disproportionation of olefinic hydrocarbons comprising a physical mixture of a disproportionation catalyst comprising a heavy metal selected from molybdenum, tungsten, rhenium and mixtures thereof, deposited on an inorganic oxide support, and a double bond isomerization catalyst comprising an acidic zeolite capable of effecting double bond isomerization, and such a process using said catalyst composition.

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(54) **Concurrent isomerization and disproportionation of olefins.**

(57) A catalyst composition for use in a process for the concurrent isomerization and disproportionation of olefinic hydrocarbons comprising a physical mixture of a disproportionation catalyst comprising a heavy metal selected from molybdenum, tungsten, rhenium and mixtures thereof, deposited on an inorganic oxide support, and a double bond isomerization catalyst comprising an acidic zeolite capable of effecting double bond isomerization, and such a process using said catalyst composition.

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CONCURRENT ISOMERIZATION AND DISPROPORTIONATION OF OLEFINS

The present invention relates to the concurrent isomerization and disproportionation of olefinic hydrocarbons utilizing a physical mixture of a disproportionation catalyst and a double bond isomerization catalyst.

Reactions of olefinic molecules in the presence of metal-containing catalysts to produce other olefinic molecules are known in the art as "disproportionation" reactions. The olefin disproportionation reaction can be visualized as the breaking of two existing double bonds between the first and second carbon atoms, and between the third and fourth carbon atoms, respectively, and the formation of two new double bonds, such as between the first and third carbon atoms and the second and fourth carbon atoms, respectively. A typical olefin disproportionation process is illustrated by U.S. Patent No. 3,261,879, wherein two similar non-symmetrical molecules of an olefin react in the presence of certain catalysts to produce one olefin of a higher carbon number and one olefin of a lower carbon number such as, for example, propylene disproportionation by the process of U.S. Patent No. 3,261,879 to produce ethylene and butylenes.

As used in this application, disproportionation process means the conversion of olefinic hydrocarbons into similar olefinic hydrocarbons of higher and lower numbers of carbon atoms per molecule. Where the reactant comprises 1- or 2-olefins having relatively long chains, a mixture of products is obtained comprising primarily olefins having both a larger and a smaller number of carbon atoms than the feed olefin but also including other disproportionated products, for example, saturated hydrocarbons, and other converted and unconverted material. Such an operation is useful in many instances. For example, a more plentiful hydrocarbon can be converted to a less plentiful and therefore more valuable hydrocarbon. One instance of such a conversion occurs when the process of this invention is used to convert both higher and lower molecular weight olefins to olefins in the C_{10} - C_{16} range, a range of olefins especially suitable for the manufacture of detergents. Another instance of a disproportionation reaction having considerable value is the disproportionation of propylene to produce ethylene and butene.

A variety of catalysts have been employed for conducting disproportionation reactions, such as those disclosed in U.S. Patent Nos. 3,340,322, 3,637,892, 3,760,026, 3,792,108 and 3,872,180, and British Patent Specification No. 1,128,091.

It is also known that the presence of a catalyst which possesses double bond isomerization activity in a disproportionation zone is advantageous because it increases the rate of conversion and makes possible the production of a wider range of reaction products. For example, the presence of such double bond isomerization activity greatly increases the disproportionation rate of symmetrical olefins such as butene-2. In addition, the isomerization activity permits the exhaustive cleavage of high molecular weight monoolefins with ethylene to lower molecular weight monoolefins such as propylene and isobutene. British Patent No. 1,205,677 provides a catalyst which comprises an olefin disproportionation component and a Group VIII noble metal double bond isomerization component, i.e., palladium, platinum or ruthenium. Another catalyst system which accomplished the same results is obtained by physically mixing catalytic magnesium oxide with tungsten oxide on silica catalyst. Other catalysts which have been developed include those obtained by copromoting an olefin disproportionation catalyst such as tungsten oxide on silica with minor amounts of the oxides of niobium, tantalum, or vanadium to provide the double bond isomerization activity.

U.S. Patent No. 3,786,112 discloses a catalyst comprising a physical mixture of an olefin disproportionation catalyst and a double bond isomerization catalyst wherein the double bond isomerization catalyst has been treated with an alkali metal or alkaline metal earth compound.

U.S. Patent No. 4,180,524 discloses a single catalyst composition containing a support, uranium and at least one of molybdenum, tungsten or rhenium, which provides double bond isomerization activity as well as olefin disproportionation activity.

The catalyst in the above references for isomerization and combined isomerization/disproportionation have either basic or neutral isomerization components. It has been found in the present invention that an acidic isomerization component in combination with a disproportionation component can be used for concurrent isomerization/disproportionation with a low side-product make, thus resulting in a greater quantity of useful olefins.

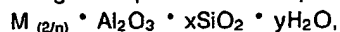
In accordance with the present invention there is provided a catalyst composition for the concurrent disproportionation and isomerization of olefinic hydrocarbons comprising a physical mixture of a disproportionation catalyst comprising a heavy metal selected from molybdenum, tungsten, rhenium and mixtures thereof, deposited on an inorganic oxide support, and a double bond isomerization catalyst comprising an acidic zeolite capable of effecting double bond isomerization.

In accordance with the present invention there is also provided a process for the concurrent isomerization and disproportionation of olefinic hydrocarbons having carbon numbers ranging from C_2 to C_{100} which

comprises contacting said olefinic hydrocarbons with such a catalyst composition.

It has been found that the physical mixture catalyst of the present invention results in improved product conversion yield and/or selectivity in a combined olefin isomerization/disproportionation process when compared to a conventionally prepared catalyst useful for disproportionation. In an olefin production process combining the steps of oligomerization, isomerization and disproportionation such as that disclosed in U.S. Patent No. 3,726,938, it is preferred to use catalysts prepared according to the present invention in the disproportionation zone.

As used herein, "zeolite" refers to a crystalline aluminosilicate with a framework based on an extensive three-dimensional network of oxygen ions. Situated within the tetrahedral sites formed by the oxygen can be either a Si(+4) or an Al(+3) ion. The $\text{AlO}_2(-)$ tetrahedra in the structure determine the framework charge. A representative empirical formula for a zeolite is written as:



where M represents the exchangeable cations, generally from the group I or II ions, although other metal, nonmetal and organic cations may also be used to balance the framework charge and n represents the cation charge. These cations are present either during synthesis or through post-synthesis ion exchange. The value of x is equal to or greater than 2 because Al (+3) does not occupy adjacent tetrahedral sites. The crystalline framework structure contains voids and channels of discrete size with pore or channel openings ranging from 3 Å to 8 Å, depending on the structure. Typical cations include: the alkali and alkaline earth cations, ammonium, tetramethylammonium and other nitrogen-containing organic cations, and the rare earth and noble metal ions. As used herein, "acidic zeolite" refers to those zeolites where the charge balancing cation is a proton, H(+).

Olefins which are subjected to concurrent isomerization and disproportionation according to the process of the present invention include C_3^+ olefinic hydrocarbons or C_3^+ internal olefins in combination with ethylene. A useful group of feed materials are olefinic hydrocarbons having carbon numbers ranging from C_2 to about C_{100} and mixtures thereof, preferably from C_2 to about C_{60} and mixtures thereof, and more preferably linear olefinic hydrocarbons having carbon numbers ranging from about C_4 to about C_{40} and mixtures thereof. Examples of compounds most suitable for disproportionation according to the present invention are acyclic 1- and 2-alkenes, and alkyl and aryl derivatives thereof having from 3 to 20 carbon atoms per molecule. Some specific examples of such olefins are propylene, 1-butene, 2-butene, 1-pentene, 2-pentene, 1-hexene, 2-heptene, 1-octene, 2-nonene, 1-dodecene, 2-tetradecene, 1-hexadecene, 2-methyl-1-butene, 2-methyl-2-butene, 3-methyl-1-butene, 1-phenylbutene-2, and 3-heptene. Higher disproportionation conversions and wider product distributions are obtained at comparable reaction times with 1-olefins than with 2-olefins. 3-olefins are disproportionated at still lower rates.

The feed should be essentially free of impurities which adversely affect the reaction. A subsequent reactivation of the catalyst to remove the effect of such impurities can be made repeatedly by heat treatment with air, using an inert gas to control burn-off temperature.

The physical mixture catalyst of the present invention is prepared by combining a supported disproportionation catalyst containing an element selected from the group consisting of molybdenum, tungsten, rhenium and mixtures thereof, and optionally cobalt, and a double bond isomerization catalyst comprising an acidic zeolite.

The disproportionation catalyst preferably comprises molybdenum and/or tungsten and/or rhenium supported on an alumina-containing support. The catalyst also preferably contains cobalt. Any conventional catalytic grade of alumina including the beta or gamma forms can be used. The catalyst can contain other materials which do not substantially promote undesirable side reactions. For example, an alumina support or base can contain silica, magnesia, titania or other bases in amounts which do not change the essential characteristics of the reaction.

The disproportionation catalyst can be prepared by any conventional method such as dry mixing, coprecipitation or impregnation. For example, a 10-100 mesh alumina can be impregnated with an aqueous solution containing molybdenum salts, such as ammonium dimolybdate and optionally, cobalt salts, such as cobalt nitrate.

In a preferred embodiment, the disproportionation catalyst in the present invention is a cobalt/molybdenum catalyst prepared by impregnating alumina with an impregnation solution combining an aqueous cobalt solution and an aqueous molybdenum solution. The cobalt solution consists of cobalt salts dissolved in water. A wide range of cobalt compounds are suitable, such as cobalt nitrate, cobalt hydroxide, cobalt acetate, cobalt oxalate, or cobalt oxide, with cobalt nitrate being preferred. The molybdenum solution consists of a water-soluble source of molybdenum oxide such as ammonium heptamolybdate or ammonium dimolybdate dissolved in water. Hydrogen peroxide may also be used to aid in solution preparation in some cases. A preferred method for preparing the molybdenum solution consists of adding hydrogen peroxide to

the solution in the range of about 0.1 to about 1.0 mole of hydrogen peroxide per mole of molybdenum. Optionally, a suitable soluble amine compound such as monoethanolamine, propanolamine or ethylenediamine may be added to the molybdenum solution in order to aid in stabilization of the solution.

Following impregnation, the resulting material is dried and calcined. Drying is accomplished by conventional means. It may be carried out by forced draft drying, vacuum drying, air drying or similar means. Drying temperatures are not critical and depend upon the particular means utilized for drying. Drying temperatures will typically range from about 50° C to about 150° C.

After drying, the material is calcined to produce the finished catalyst. The material may be calcined in an oxidizing or neutral atmosphere, although air is preferred. However, if binders and/or lubricants are used the material is heated in an oxygen-containing atmosphere, preferably air, in order to burn out the binders and lubricants. Calcining temperatures will typically range from about 300° C to about 600° C. Burn-out temperatures will depend on the concentration of oxygen in the burn-out atmosphere as well as the burn-out time involved. Typically, burn-out temperatures will range from about 300° C to about 600° C. Drying, calcining and burn-out may be combined in one or two steps. Most frequently the calcining and/or burn-out steps are combined using an oxygen-containing atmosphere.

The final catalysts typically contain from about 5 percent by weight to about 18 percent by weight molybdenum, about 8 percent by weight to about 32 percent by weight tungsten or from about 1 percent by weight to about 20 percent by weight rhenium. When mixtures of molybdenum, and tungsten and rhenium are utilized, the final catalyst typically contains from about 5 percent by weight to about 32 percent by weight molybdenum and/or tungsten and/or rhenium. When the catalyst contains cobalt, the final catalyst contains from about 0.1 percent by weight to about 5 percent by weight cobalt. These types of catalysts are well known in the art and can be prepared according to the prior art, such as but not limited to aforementioned U.S. Patent No. 3,261,879 and U.S. Patent No. 3,365,513.

The double bond isomerization catalysts which are suitable for use in the present invention are acidic zeolites. Suitable acidic zeolite include ferrierite, ZSM-35, ZSM-5, mordenite and fujasite. In a preferred embodiment, the acidic zeolite catalyst is ferrierite. Ferrierite is a naturally occurring zeolite mineral having a composition which varies somewhat with the particular source.

The prominent structural features of ferrierite have been found by X-ray crystal determination to be parallel channels in the aluminosilicate framework. The ferrierite is a two dimensional zeolite consisting of intersecting 8 and 10 ring channels. The larger 4.3 Å x 5.5 Å ten ring channel parallels the c crystallographic axis, while the smaller 3.4 Å x 4.8 Å eight ring channel parallels the b crystallographic axis. Practically speaking, the larger ten ring channel is the only diffusion path available to a molecule of any moderate size. Therefore, the channel system of ferrierite is essentially undimensional due to practical considerations.

Suitable ferrierite catalysts are exemplified by the ZSM-35 aluminosilicate of U.S. Patent No. 4,016,245 or most preferably by a piperidine derived ferrierite as discussed in U.S. Patent No. 4,251,499. Ferrierite aluminosilicate catalysts are typically prepared by in the manner described in U.S. Patent No. 4,251,499, in which an aqueous mixture having one or more compounds of an alkali metal, one or more aluminium compounds, one or more silicon compounds and at least one compound selected from piperidine and alkyl-substituted piperidine is formed and maintained at a temperature of 100° C to 200° C until the ferrierite has formed, followed by recovery of the ferrierite crystals.

In one embodiment, the ferrierite catalyst is treated with methylsilylating agents or organofunctional silylating or silane agents in order to reduce undesirable dimerization reactions which often accompany olefin isomerization. These agents are believed to be responsible for modifying the catalyst sites on the ferrierite aluminosilicate surface and thereby reducing access to dimerization sites for the olefin feed material. A list of suitable silylating agents is set forth in Kirk-Othmer, vol. 18 at pages 260-268. A non-limiting list of suitable silylating agents includes 1,1,1,3,3,3-hexamethyldisilazane, tetraethoxysilane, trimethylchlorosilane, n-trimethylsilylacetamide, tetramethyldisilazane, bis(trimethylsilyl)acetamide, vinyltriacetoxysilane, dimethylchlorosilane, bromomethyldimethylchlorosilane, di(chloromethyl)-tetramethyldisilazane and vinyltriethoxysilane, with 1,1,1,3,3,3-hexamethyldisilazane being preferred.

The catalyst of the present invention is prepared by admixing the disproportionation catalyst and the double bond isomerization catalyst. To facilitate mixing, it is desirable to have the catalysts in a form which is compatible one with the other. The catalysts may be, for example, in the form of powders, extrudates or pills prior to mixing the two catalysts together. The amount of disproportionation catalyst used in the physical catalyst mixture is generally in excess of the amount of double bond isomerization catalyst used in the mixture. Preferably the ratio of disproportionation catalyst to double bond isomerization catalyst in the physical mixture is from about 50:1 to about 0.02:1, preferably from about 25:1 to about 0.5:1, and more preferably, from about 10:1 to about 1:1. Particularly preferred is a 9:1 ratio of disproportionation catalyst to

double bond isomerization catalyst in the physical mixture.

The physical mixture catalyst system must be activated prior to use in the combined isomerization/disproportionation process. Although each of the individual catalysts can be activated prior to mixing the two catalysts together, it is preferred that the catalyst system be activated after the disproportionation catalyst and isomerization catalyst have been admixed and placed in a suitable reactor. While activation is usually accomplished by contacting the physical mixture catalyst system with an oxygen-containing gas at elevated temperatures, other activation methods such as heating under a vacuum, or contact with various gases such as nitrogen or argon at high temperatures, can be used. The temperature, contact times, and other conditions of activation have been reported in the prior art and are generally the same conditions which are utilized to activate a disproportionation catalyst. Typically, the activation conditions include a temperature in the range of from about 300 °C to about 900 °C for about 30 minutes to about 24 hours.

The combined isomerization/disproportionation process of the present invention can be carried out either batchwise or continuously, using a fixed catalyst bed, or a stirrer equipped reactor or other mobile catalyst contacting process as well as any other well known contacting technique. Preferred reaction conditions, e.g., temperature, pressure and flow rates, vary somewhat depending upon such factors as the specific catalyst composition, the particular feed olefin and desired products. The process is carried out at temperatures ranging from about 10 °C to about 350 °C and at pressures in the range of about 446 kPa (50 psig) to about 3549 kPa (500 psig). The isomerization/ disproportionation reaction is usually effected in a liquid phase in the presence of a small amount of ethylene and if desired, liquid reaction diluents are utilized. Examples of suitable diluents are hydrocarbons free from aliphatic unsaturation, such as acyclic or alicyclic alkanes of from 6 to 12 carbon atoms, i.e. hexane, isooctane and cyclohexane. Also exemplary would be monoaromatic compounds such as benzene and toluene. If the diluent is added, it is present in amounts up to 20 moles of diluent per mole of olefinic reactants.

The operable range of contact time for the process of the present invention depends primarily upon the operating temperature and the activity of the catalyst, which is influenced by such factors as surface area, promoter concentration and activation temperature. In general, the distribution of products is not drastically altered by variation in contact time. Shorter contact times are usually associated with higher temperatures, but, when larger amounts of higher molecular weight products are desired, a suitable combination of contact time and temperature is selected. With proper selection of conditions and contact times, very high efficiency of conversion to desired products can be obtained.

In this application, space rates are given in WHSV (weight hourly space velocity; weight of reactant feed per weight of catalyst per hour).

With a fixed bed reactor, continuous flow operation at pressures in the range of about 446 kPa (50 psig) to about 3549 kPa (500 psig), preferably about 1136 kPa (150 psig) to about 1825 kPa (250 psig), with catalysts having densities ranging from about 0.5 gram per cc to about 1.0 gram per cc and surface areas greater than about 300 m²/g, and at temperatures in the range of about 10 °C to about 350 °C, preferably about 100 °C to about 250 °C, weight hourly space velocities in the range of about 0.1 to about 10.0 parts by weight of olefinic hydrocarbon feed per part by weight of catalyst per hour are suitable. The space velocity is adjusted according to changes in density of feed due to change of pressure or temperature, and variation in reaction temperature and the activity of the catalyst. The higher space velocities in general are associated with higher reaction temperatures.

The physical mixture catalyst system of the present invention is advantageous with respect to a catalyst system in which the olefin feed is only disproportionated rather than isomerized and disproportionated concurrently in that a different mixture of product olefins is obtained. The ability to shift the mixture of product olefins is particularly useful in maximizing the economic return from any given olefin feedstock.

The process of the present invention will be further described by reference to the following Examples.

Examples

50

Catalyst Preparation

Catalyst A

55 Catalyst A is a physical mixture of a cobalt/molybdenum disproportionation catalyst and a ferrierite aluminosilicate double bond isomerization catalyst.

The disproportionation catalyst was prepared using a conventional dry pore volume impregnation technique. A solution suitable for impregnating 75 grams of calcined alumina support with a pore volume of

0.69 cm³/g was prepared as follows. An impregnation solution was made by combining 5.78 grams of cobalt nitrate, 12.86 grams of ammonium dimolybdate and enough 24% aqueous ammonia to bring the solution to a total volume of 51 ml. After adding the entire solution to the alumina support in several small portions with intermediate agitations, the impregnated support was dried overnight at 150 °C and calcined in air for 2 hours at 450 °C.

The double bond isomerization catalyst was prepared by incorporation of the organic base, piperidine, with stirring into a solution of sodium water glass (28% SiO₂, 8% Na₂O) in water. To the mixture thus obtained was added a solution of aluminum sulfate in water or a mixture of water and sulfuric acid with stirring. The targeted molar composition for the starting mixture was 93.5 SiO₂; 4 Al₂O₃; 10 Na₂O; 17 Na₂SO₄; 36.7 piperidine; and 1938 H₂O. The resultant mixture was stirred for another 15 minutes and then maintained at a temperature of 150 °C for at least 25 hours. The solid product was isolated from the reaction mixture. The resultant solid product was exchanged twice with an aqueous 2M solution of NH₄NO₃ to yield ammonium ferrierite. The ammonium ferrierite was converted to hydrogen ferrierite by calcination in air for two hours at a temperature of at least 300 °C.

The two catalysts were then mixed by adding nine parts of the disproportionation catalyst to one part of the double bond isomerization catalyst, followed by agitation to produce a uniform mixture of the two catalysts. The properties of the catalyst are listed in Table I.

Catalyst B

Catalyst B was prepared in a manner similar to Catalyst A except that the ferrierite aluminosilicate catalyst was silylated prior to admixing with the cobalt/molybdenum catalyst utilizing the following silylation procedure. A total of 12.1 grams of ammonium ferrierite as 16-45 mesh powder was refluxed in hexane along with 8 grams of 1,1,1,3,3,3-hexamethyldisilazane for 1 to 2 hours. The silylated ferrierite was then washed with hexane and dried under N₂ at 120 °C for 16 hours. The properties of the catalyst are listed in Table I.

Catalyst C

Catalyst C is a conventional disproportionation catalyst prepared using a conventional dry pore volume impregnation technique. A solution suitable for impregnating 75 grams of calcined alumina support with a pore volume of 0.69 cm³/g was prepared as follows. An impregnation solution was made by combining 5.78 grams of cobalt nitrate, 12.86 grams of ammonium dimolybdate and enough 24% aqueous ammonia to bring the solution to a total volume of 51 ml. After adding the entire solution to the alumina support in several small portions with intermediate agitations, the impregnated support was dried overnight at 150 °C and calcined in air for 2 hours at 450 °C. The properties of the catalyst are listed in Table I.

Catalyst Testing

Catalysts A, B, and C were each tested utilizing the following procedure. 20 cm³ of 16-45 mesh catalyst particles diluted 1/1 with 80 mesh SiC are charged to a stainless steel reactor to obtain a bed length of 8 inches. The catalyst is heated at a temperature of 550 °C under flowing nitrogen for 12 hours to remove any residual water from the catalyst. The catalyst is then cooled to 121 °C (250 °F) and feed is introduced at a weight hourly space velocity (WHSV) of about 1.5. The feed for these reactions is an equilibrium mixture of decenes prepared by the isomerization of 1-decene. The feed contains approximately 1.5% branched decenes. The results of catalyst testing are presented in Table II.

As mentioned previously, the physical mixture catalysts prepared by the process of the present invention have improved conversion rates and a wider range of reaction products than conventional disproportionation catalysts in a disproportionation reaction zone. The data in Table II shows the carbon number distributions for Catalysts A, B and C. It is evident from these data that Catalyst A yields a comparable amount of C₃-C₈ olefin product, less C₉-C₁₄ olefin product and more C₁₅-C₂₈ olefin product than the standard, Catalyst C. Catalyst B yields a comparable amount of C₂-C₅ olefin product, less C₆-C₁₂ olefin product and more C₁₃-C₂₈ olefin product than the standard, Catalyst C. The general effect of both Catalyst A and B is to shift the overall olefin product distribution to favor heavier olefins versus the product obtained with the standard, Catalyst C. Catalyst A yields a slightly lighter olefin product as compared with Catalyst B because of differences in the pretreatment of the isomerization catalyst function, specifically, silylation.

TABLE I
Catalyst Properties

5	Catalyst	<u>A</u>	<u>B</u>	<u>C</u>
10	Ratio Disp. Catalyst/ Isom. Catalyst	9:1	9:1	_____
	Grams Disp. Catalyst	12.1	12.0	13.4
	Grams Isom. Catalyst	0.9	1.1	_____
15	Disp. Catalyst Composition			
	%wt Mo ^{a)}	8.1	8.1	8.1
20	%wt Co ^{b)}	3.2	3.2	3.2
	Isom. Catalyst	H ⁺	Si-H ⁺	
	Composition	Ferrierite	Ferrierite	_____

a) Weight percent determined by neutron activation analysis or atomic absorption spectroscopy.

b) Weight percent determined by neutron activation analysis or atomic absorption spectroscopy.

TABLE IICatalyst Test Results

Catalyst	A	B	C
C ₁₀ Feed	Iso. C ₁₀	Iso. C ₁₀	Iso. C ₁₀
Reaction			
Temperature, °C (°F)	121 (250)	121 (250)	121 (250)
Catalyst Hours	3	2.75	3
Catalyst Volume, cm ³	20	20	20
Catalyst Weight, gm	13.4	13.4	13.4
WHSV	1.8	1.4	1.5

Carbon Number Distribution

Catalyst	A	B	C
C ₂	0.000	0.000	0.000
C ₃	0.045	0.032	0.027
C ₄	1.126	0.075	0.743
C ₅	2.214	1.387	1.646
C ₆	4.189	2.626	3.574
C ₇	5.925	3.787	5.693
C ₈	7.584	5.227	8.166
C ₉	9.086	7.195	10.542
C ₁₀	11.356	9.555	13.817
C ₁₁	10.283	10.443	13.053
C ₁₂	9.768	10.921	12.281
C ₁₃	8.700	10.621	10.345
C ₁₄	7.437	9.786	8.091
C ₁₅	5.970	8.198	5.462
C ₁₆	4.540	6.325	3.290
C ₁₇	3.346	4.766	1.454
C ₁₈	2.514	3.456	0.721
C ₁₉	2.116	2.222	0.414
C ₂₀	1.205	1.154	0.245
C ₂₁	0.819	0.670	0.243

5	C ₂₂	0.559	0.418	0.057
	C ₂₃	0.371	0.256	0.063
	C ₂₄	0.238	0.151	0.026
	C ₂₅	0.175	0.115	0.018
10	C ₂₆	0.276	0.215	0.012
	C ₂₇	0.157	0.113	0.011
	C ₂₈	0.000	0.000	0.007
15				

Claims

- 20 1. A catalyst composition for the concurrent disproportionation and isomerization of olefinic hydrocarbons comprising a physical mixture of a disproportionation catalyst comprising a heavy metal selected from molybdenum, tungsten, rhenium and mixtures thereof, deposited on an inorganic oxide support, and a double bond isomerization catalyst comprising an acidic zeolite capable of effecting double bond isomerization.
- 25 2. A catalyst composition according to claim 1 wherein said disproportionation catalyst additionally contains cobalt.
- 30 3. A catalyst composition according to claim 2 wherein said disproportionation catalyst contains from 0.1 percent by weight to 5 percent by weight cobalt.
4. A catalyst composition according to claim 3 wherein said disproportionation catalyst contains from 2.5 percent by weight to 4 percent by weight cobalt.
- 35 5. A catalyst composition according to claim 1, 2, 3 or 4 wherein said acidic zeolite is ferrierite.
6. A catalyst composition according to any one of the preceding claims wherein a ratio of disproportionation catalyst to double bond isomerization catalyst in the range of from 50:1 to 0.02:1 is used.
- 40 7. A catalyst composition according to claim 6 wherein a ratio of disproportionation catalyst to double bond isomerization catalyst in the range of from 25:1 to 0.5:1 is used.
8. A catalyst composition according to any one of the preceding claims wherein said disproportionation catalyst contains from 1 percent by weight to 32 percent by weight heavy metal.
- 45 9. A catalyst composition according to claim 8 wherein said disproportionation catalyst contains from 5 percent by weight to 18 percent by weight molybdenum.
- 50 10. A process for the concurrent disproportionation and isomerization of olefinic hydrocarbons having carbon numbers ranging from C₂ to C₁₀₀ which comprises contacting said olefinic hydrocarbons with a catalyst composition according to any one of claims 1 to 9.
- 55 11. A process according to claim 10 wherein said process is carried out at a temperature in the range of from 10° C to 350° C and a pressure in the range of from 446 kPa (50 psig) to 3549 kPa (500 psig).



European
Patent Office

EUROPEAN SEARCH REPORT

Application Number

EP 90 20 3260

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.5)
Y	US-A-4 727 203 (D.M. HAMILTON) * Abstract; column 4, lines 17-32; column 4, line 60 - column 5, line 19; claims 1-34 *	1-11	B 01 J 37/04 B 01 J 29/36 C 07 C 6/04

D,Y	US-A-3 786 112 (REUSSEN et al.) * Abstract; column 3, lines 1-22; claims 1-14 *	1-11	

D,A	GB-A-1 205 677 (ICI)		

A	US-A-4 575 575 (DRAKE et al.)		

A	AU-B-4 711 9 (STANDARD OIL)(1979)		

			TECHNICAL FIELDS SEARCHED (Int. Cl.5)
			B 01 J C 07 C
The present search report has been drawn up for all claims			
Place of search		Date of completion of search	Examiner
The Hague		28 March 91	LO CONTE C.
CATEGORY OF CITED DOCUMENTS			
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P: intermediate document		&: member of the same patent family, corresponding document	
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